State of The Art of MBR Technology and Its Perspective in Japan

Hiroki ITOKAWA^{*} Research and Technology Development Division, Japan Sewage Works Agency (JS)

1. Introduction

Membrane bioreactor (MBR) technology is characterized as a combination of biological wastewater treatment (WWT) and membrane separation, by which biomass can retained in the system without conventional gravity sedimentation. This leads to well-characterized advantages of the technology over conventional activated sludge processes, including smaller reactor footprint, excellent effluent quality, and smaller sludge production (Judd, 2006). MBR has been successfully installed worldwide, not only for small-scale industrial wastewater treatment plants (WWTPs), but also for larger-scale municipal WWTPs (Yang *et al.*, 2006). Japan has been playing an important role in this field, especially by pioneering works regarding submerged MBR systems, as well as developments of a variety of commercial membrane systems.

In this short paper, development and installation of MBR systems in Japan, as well as ongoing R&D projects, are summarized particularly focusing on the application to municipal WWTPs.

2. Development of municipal MBRs in Japan

In Japan, full-scale commercial MBRs started to be installed in early 1980s, as an external cross-flow system. At that time, the principal target was a building-scale wastewater recycling system, which had been motivated by some local governments. As for domestic wastewater treatment, MBR has been used since 1985 for on-site individual house- to district-scale WWT system "*johkaso*". Especially after the "invention" of submerged MBR in late 1980s, MBR market for *johkaso* system has grown rapidly, and the number of installations is, at present, not less than 1,500. MBR has been also installed in nightsoil treatment plants and other small-scale domestic WWTPs since late 1980s, as well as installation to a number of industrial WWTPs.

In contrast to these small-scale WWT systems, application of MBR to larger-scale municipal WWTPs was behind the international trend, where in

^{*} 5141 Shimosasame, Toda City, Saitama 335-0037, Japan e-mail: itokawah@jswa.go.jp

1998 the first full-scale plant was commissioned in UK. In the same year, Japan Sewage Works Agency (JS) launched a R&D project on MBR system development and evaluation for municipal WWTPs. Pilot-scale studies were conducted with four private companies with different membrane systems; two flat sheet (Kubota and Hitachi-Plant) and two hollow fibre (Zenon and Mitsubishi-Rayon) systems. According to the results of the project, in 2003, JS published "MBR Design Recommendations", in which system configuration and design

Parameters	Design recommendation	
Target capacity	200 - 3,000 m ³ /d	
Inflow equalization	Prerequisite	
Pre-screen	1 mm of opening	
Bioreactor configuration	MLE (Pre-denitrification)	
Anoxic HRT	3 hr	
Aerobic HRT	3 hr	
Internal recycle	200%	
Membrane system	Submerged, integrate	

Table 2 Municipal MBRs operated in Japan

Name		Operated since	Capacity		Mem.
			Present	Future	Туре
1	Fukusaki	Mar 2005	2,100	12,600	FS
2	Kobugahara	Apr 2005	240	240	FS
3	Yusuhara	Dec 2005	400	800	FS
4	Okutsu	Apr 2006	600	600	HF
5	Daitocho	Sep 2006	1,000	2,000	FS
6	Tohro	Mar 2007	125	125	FS
7	Kaietsu	Apr 2007	230	230	HF
8	Jousai	Mar 2008	1,375	1,375	HF
9	Heda	Mar 2008	2,140	3,200	FS

parameters were specified (Table 1). An important feature of the document is that it shows universal design materials for small-scale municipal MBR (less than 3,000 m^3/d), including dimensioning of bioreactors and system arrangement plans, which can be used for any of four membrane systems (one more hollow fibre system from Asahi-Kasei was entitled in 2005). At the same time, JS carried out 2nd phase pilot-scale studies (2001-2004) with five membrane systems, particularly focusing on the reduction of operating costs. Based on these R&D projects and the design materials, the first full-scale municipal MBR was constructed and commissioned in March 2005 (Fukusaki WWTP; 2,100 m^3/d).

3. Installation of municipal MBRs in Japan

As of the end of 2008, MBRs are operated in 9 municipal WWTPs in Japan, whose capacity ranges from 125 to 2,100 m³/d (Table 2). Six of them use flat sheet membrane and the others use hollow fibre membrane. According to the JS Design Recommendations, all the plants were designed for pre-denitrification system, in which membrane units were submerged in oxic tanks (integrated system).

4. Ongoing project for larger-scale application

Internationally, there is a trend in MBR market for larger-scale application. Actually, some MBR plants are being constructed/planned whose capacity

exceeds 100,000 m³/d in US and even over 200,000 m³/d in the Middle East. Considering these circumstances, JS started the 3rd phase pilot-scale project in 2006 toward MBR application to larger-scale municipal WWTPs (more than 10,000 m³/d). The following points are particularly concerned.

(1) New membrane systems/modules: Some new membrane modules, developed for larger-scale installations, are tested. In addition, a new external MBR system with ceramics membrane from Metawater is evaluated.

(2) Variety of reactor configuration: In contrast to the fixed system configuration based on the present Design Recommendations (MLE with integrated submerged membrane), a MBR system for larger-scale WWTPs has to be more flexible, since the most of the case would be for up-grade of existing WWTPs. On this basis, a variety of system configurations are tested including separate/ external systems, incorporation of EBPR, and the use of primary sedimentation.

(3) New cleaning strategies: An increase in membrane modules in larger-scale MBRs requires more efficient chemical cleaning strategies with less labor. Although the approaches are different among membrane suppliers, new cleaning methods are tested in pilot plants (e.g. automated recovery cleaning, optimization of chemical dose).

(4) Post-treatment for reuse purpose: In order to cope with more stringent reuse requirements, post-treatment systems of MBR effluent using NF/RO membrane are experimentally evaluated and optimized for different kinds of commercial membranes.

5. Future perspective

Although we have almost 30 years of MBR application, we are still on "small-scale" stage concerning installation to municipal WWTPs. More promotion would be necessary to let the technology to be accepted by rather conservative plant operators. On this basis, the Ministry of Land, Infrastructure and Transport has started to prepare a guideline for membrane technology with through discussion in specific committee. In addition, MBR installation to an existing WWTP with 60,000 m³/d of capacity is now under planning stage. This project will be a touchstone for the future of MBR technology in Japan. Re-consideration of urban water management, together with innovative water reuse scheme, will also favor the technology.

References

Judd,S. (2006) The MBR Book: Principles and Applications of Membrane Bioreactors in Water and Wastewater Treatment. Elsevier, Oxford.

Yang,W., Cicek,N. and Ilg,J. (2006) State-of-the-art of membrane bioreactors: Worldwide research and commercial applications in North America. *Journal of Membrane Sciences*, 270, 201-211.



Membrane bioreactor (MBR)

MBR: A combination of biological WWT (e.g. activated sludge) and membrane filtration as a measure for solid-liquid separation.

> Advantages over CAS processes:

- Complete rejection of suspended solids.
- Higher MLSS (>10 g/L).
- Smaller footprint (< 6hr for BNR).
- Smaller sludge production.
- Simple monitoring parameters (e.g. TMP).
- Installed worldwide, from small-scale on-site WWTPs to large-scale municipal WWTPs.

Full-scale application to municipal WWTPs has just around ten years history.







Large MBR projects worldwide

WWTP name Location Commissioning Hydraulic capacity Jumeirah Golf Estates Dubai 2010 220,000 m³/d Palm Jebel Ali Dubai 2010 220,000 m³/d **Brightwater** USA 2010 144,000 m³/d Jebel Ali Free Zone 140,000 m³/d Dubai 2007 International City 110,000 m³/d Dubai 2007 Johns Creek USA 93,500 m³/d 2007 Beixiaohe China 2007 80,000 m³/d 78,000 m³/d Al-Ansab 2006 Oman 75,700 m³/d Peoria USA 2007 60,200 m³/d Lusail Qatar 2007 60,000 m³/d China Qinghe 2007 47,300 m³/d Syndial Italy 2007



JS pilot-scale studies (1st phase)

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> Pilot-scale study with 4 private companies (1998-2001)

- Four membranes (Kubota, Zenon, Mitsubishi Rayon and Hitachi Plant).
- Process evaluation.
- Design and operating parameters.



JS pilot-scale studies (2nd phase)

Pilot-scale study with 6 private companies (2001-2004)

- Five membranes (Kubota, Zenon, Mitsubishi Rayon, Hitachi Plant, and Asahi Kasei Chemicals).
- Reduction of operating cost by 30%.





Design guideline for municipal MBR

> JS Design Recommendations for MBR (2003)

- Fixed process configuration and design parameters.
- Even plant layout is "standardized" regardless of membrane type used.
 - * Capacity: 200 3,000 m³/d after flow equalization.



Design guideline for municipal MBR

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> JS Design Recommendations for MBR (2003)

- Universal design parameters.

Flow equalization	Prerequisite (4.6 hr, typically)
Fine screen	1 mm
Bioreactor configuration	Pre-denitrification (MLE)
Anoxic HRT	3 hr
Aerobic HRT	3 hr (membrane submerged)
MLSS	10 g/L
Internal recycle	200 % of influent

Municipal MBR installations

No	Name	Commissioning	Capacity [m ³ /d]*	Supplier
1	Fukusaki	Mar 2005	4,200 (12,600)	Kubota
2	Kobugahara	Apr 2005	240	Kubota
3	Yusuhara	Dec 2005	400 (800)	Kubota
4	Okutsu	Apr 2006	600	Zenon
5	Daitocho	Sep 2006	1,000 (2,000)	Kubota
6	Tohro	Mar 2007	125	Kubota
7	Kaietsu	Apr 2007	230	Mitsubishi
8	Jousai	Mar 2008	1,375	Asahi-Kasei
9	Heda	Mar 2008	2,140 (3,200)	Hitachi

* A value in the parentheses indicates a full-capacity in future.

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Municipal MBRs installations

Okutsu WWTP

- 600 m³/d
- GE-Zenon HF membrane





Municipal MBRs installations

Kaietsu WWTP

- 230 m³/d
- Mitsubishi HF membrane



> 3rd phase pilot-scale study with 4 private companies (2006-2009)

- Four membranes (Kubota, Hitachi Plant, Asahi Kasei Chemicals, and Metawater).
- Demonstrating systems for larger-scale installation.



Asahi Kasei Chemicals (HF)



<u>Metawater</u> (Ceramics)







Toward larger-scale installations

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It is important to design the system fit to existing facilities.
A standardized approach is no longer efficient; a variety of system configurations is required.



Toward larger-scale installations

- In the 3rd phase pilot-scale studies, the following points are particularly concerned.
- New membranes/modules (modules with higher packing density, ceramic membrane...).
- Membrane systems other than integrated ones (separated or external system).
- Optimized internal recycle.
- Incorporation of EBPR.
- Gravity filtration for FS membranes.
- Use of primary sedimentation.
- Improved chemical cleaning (automated RC, optimized doze...).
- Post RO treatment for effluent reuse

Future perspectives

- What is necessary for the FUTURE of MBR in Japan
 - Cost reduction (construction & operation)
 - Acceptance of the technology
 - Motivation for improving effluent quality/safety
 - Innovation in urban water management

Current topics

- Preparation of a guideline for membrane technology by MLIT (2008 -).
- Design of 60,000 m³/d MBR (2009 -).
- Evaluation of existing small-scale MBRs (2009 -).



effluent concentrate

MBR

effluent

